

Chemistry 163B

Refrigerators and Generalization of Ideal Gas Carnot

(four steps to exactitude)

E&R pp 86-91 *[81-85]_{2nd}*, 109-111 *[102-104]_{2nd}*; Raff pp. 159-164

statements of the Second Law of Thermodynamics

1. Macroscopic properties of an isolated system eventually assume constant values (e.g. pressure in two bulbs of gas becomes constant; two block of metal reach same T) [*Andrews. p37*]
2. It is impossible to construct a device that operates in cycles and that converts heat into work without producing some other change in the surroundings. *Kelvin's Statement [Raff p 157]; Carnot Cycle*
3. It is impossible to have a natural process which produces no other effect than absorption of heat from a colder body and discharge of heat to a warmer body. *Clausius's Statement, refrigerator*
4. In the neighborhood of any prescribed initial state there are states which cannot be reached by any adiabatic process
~ *Caratheodory's statement [Andrews p. 58]*

roadmap for second law

- ✓ 1. Phenomenological statements (what is ALWAYS observed)
- ✓ 2. Ideal gas Carnot [*reversible*] cycle efficiency of heat → work (Carnot cycle transfers heat only at T_U and T_L)
3. Any cyclic engine operating between T_U and T_L must have an equal or lower efficiency than Carnot OR VIOLATE one of the phenomenological statements (observations)
4. Generalize Carnot to any reversible cycle (E&R fig 5.4)
5. Show that for this REVERSIBLE cycle
$$q_U + q_L \neq 0 \text{ (}\vec{d}q \text{ inexact differential)}$$

but

$$\frac{q_U}{T_U} + \frac{q_L}{T_L} = 0 \text{ (something special about } \frac{\vec{d}q_{rev}}{T}\text{)}$$
6. S, entropy and spontaneous changes

goals for lecture[s]

- Carnot in reverse: refrigerators and heat pumps
- Show that $\epsilon_{\text{ideal gas rev Carnot}} \geq \epsilon_{\text{any other machine}}$ otherwise one of the phenomenological statements violated
- Not only for ideal gas but $\epsilon_{\text{ideal gas rev Carnot}} = \epsilon_{\text{any other rev Carnot}}$
- $dS \equiv \frac{\bar{d}q_{\text{reversible}}}{T}$ $\oint dS = \oint \frac{\bar{d}q_{\text{reversible}}}{T} = 0$ and S is **STATE FUNCTION**

Carnot engine arithmetic (for below table see handout) ➡

ENGINE	q	W _{sys}	W _{surr}	
I. isothermal expansion	$+nR T_U \ln \frac{P_1}{P_2}$ 1.3	$-nR T_U \ln \frac{P_1}{P_2}$ 1.2	$+nR T_U \ln \frac{P_1}{P_2}$	heat in at T _H work out
II adiabatic expansion	0	$n\bar{C}_V(T_U - T_U)$ 2.4	$-n\bar{C}_V(T_U - T_U)$	work out
III. isothermal compression	$nR T_L \ln \frac{P_3}{P_4} =$ $-nR T_L \ln \frac{P_1}{P_2}$ 3.3&T.3	$-nR T_L \ln \frac{P_3}{P_4}$ $= nR T_L \ln \frac{P_1}{P_2}$ 3.2&T.3	$-nR T_L \ln \frac{P_1}{P_2}$	heat lost at T _L work in
IV. adiabatic compression	0	$n\bar{C}_V(T_U - T_L)$ 4.4	$-n\bar{C}_V(T_U - T_L)$	work in
net gain/cost	q _{in} = q _I $+nR T_U \ln \frac{P_1}{P_2}$		W _{total} = W _I +W _{II} +W _{III} +W _{IV} = $nR(T_U - T_L) \ln \frac{P_1}{P_2}$	ε = W _{surr} /q _{in} ε = (T _U -T _L)/T _U

remember Carnot engine

- **does net work on surroundings**

and

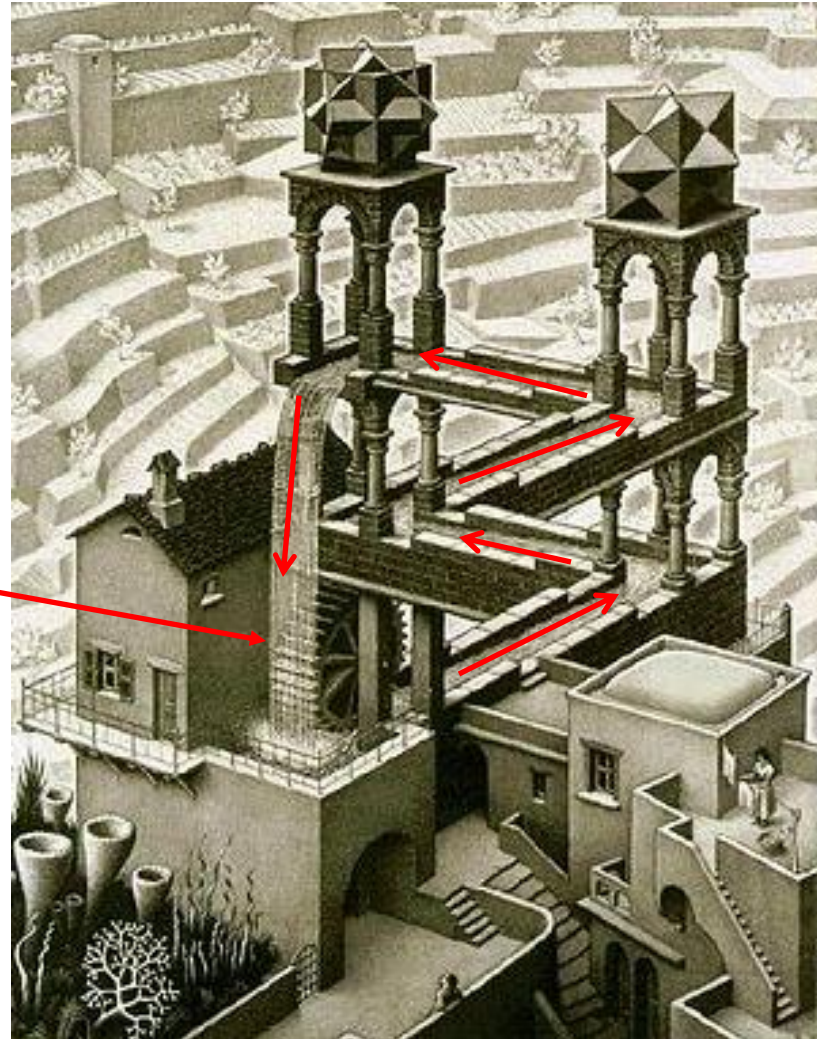
- **net heat $q_{U(I)} + q_{L(III)} = -W_{\text{total}}$**

perpetual motion of the first kind (produce work with no heat input)
Escher "Waterfall"

cyclic machine
(water 'flows downhill'
to pillar on left;
'round and 'round)
no energy input

work on surroundings

VIOLATES 1st LAW



- **does net work on surroundings**

but

- **extracts heat from surroundings at T_U**

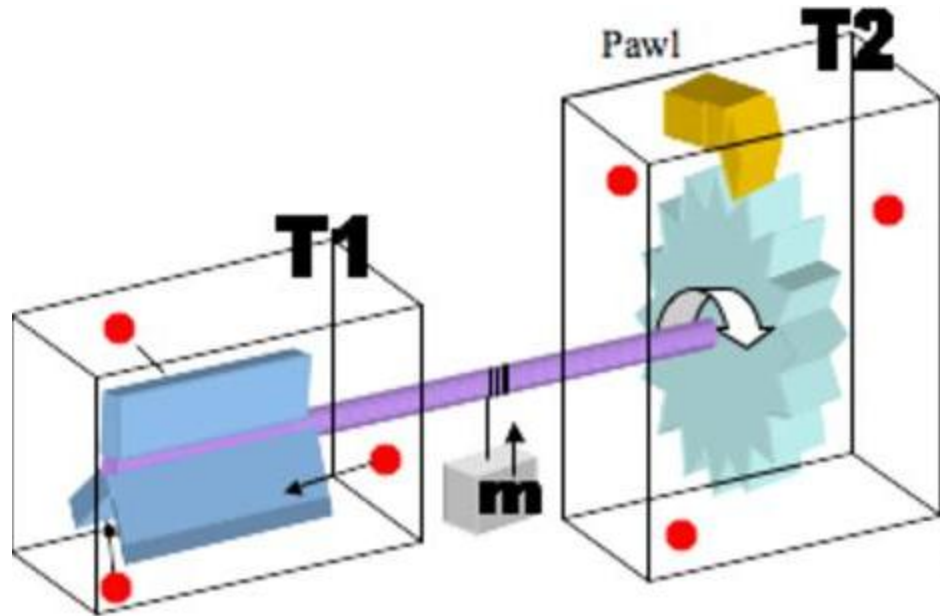
$$q_{U(I)} < 0$$

- **gives off heat to surroundings at T_L**

$$q_{L(III)} > 0$$

perpetual motion of the second kind (produce work extracting heat from cooler source to run machine at warmer temperature)

Brownian Ratchet



get work only if $T1 > T2$

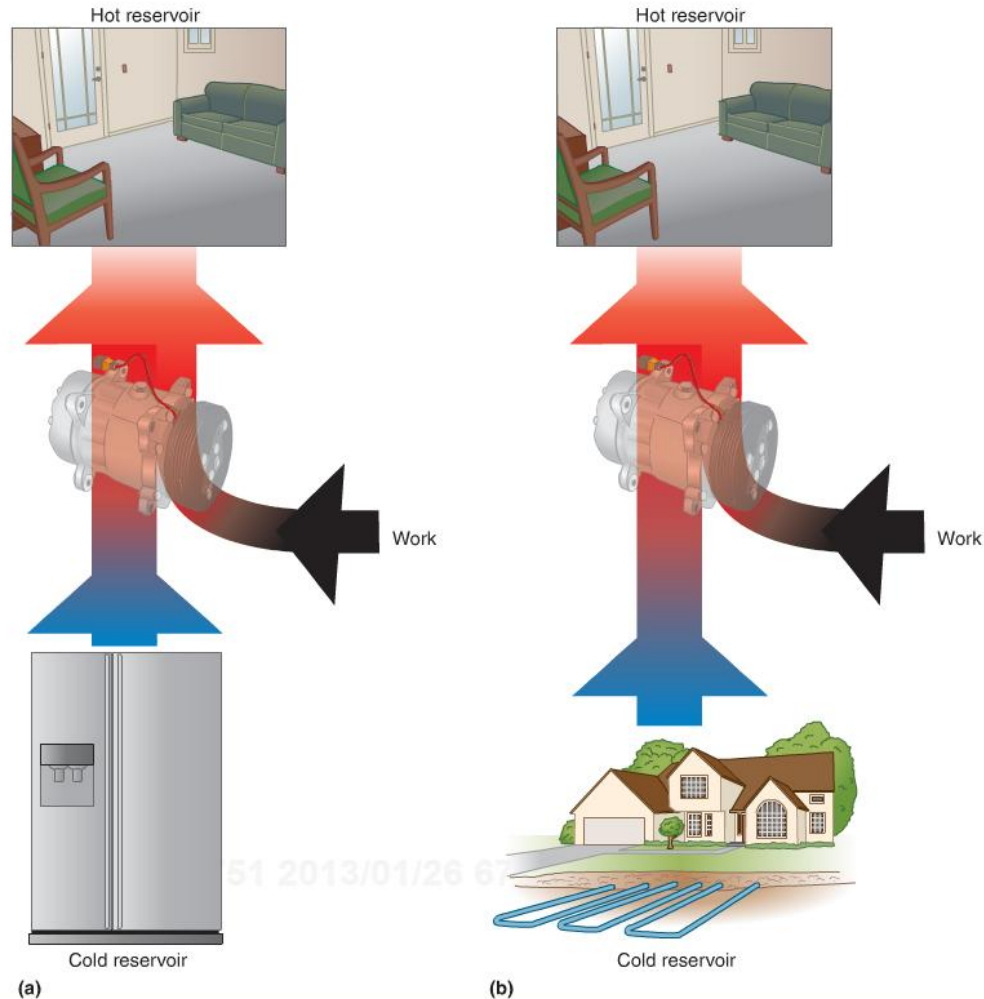
http://wapedia.mobi/en/Brownian_ratchet#1.

- it only makes 'sense' to talk about running a process in **REVERSE** for **reversible** processes (on a PV diagram there is no 'reverse' process for expansion against constant P_{ext})
- however the Carnot cycle is a combination of reversible processes

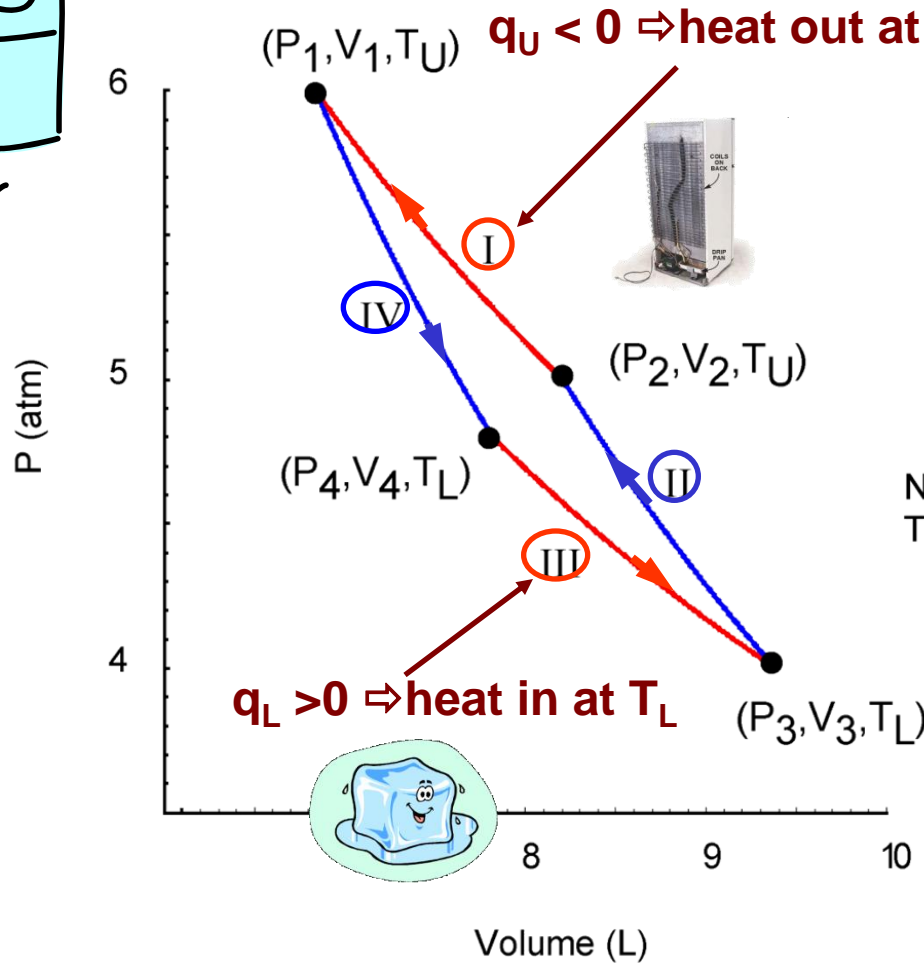
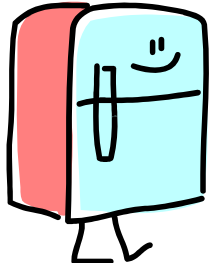
heat pumps and refrigerators (fig. 5.17 E&R) 3rd

FIGURE 5.17

Reverse heat engines can be used to induce heat flow from a cold reservoir to a hot reservoir with the input of work. **(a)** Refrigerator: the cold reservoir is the interior of a refrigerator, and the hot reservoir is the room in which the refrigerator is located. **(b)** Heat pump: the cold reservoir is water-filled pipes buried in the ground, and the hot reservoir is the interior of the house to be heated. The relative widths of the two paths entering the hot reservoir show that a small amount of work input can move a larger amount of heat from the cold to the hot reservoir. In both cases, the engine is a compressor.



reverse Carnot cycle: a refrigerator



$W_{\text{sys}} = -W_{\text{surr}} > 0$
work done ON system

$P_1 = 6 \text{ atm}, T_1 = T_U = 500 \text{ K}$

$P_2 = 5 \text{ atm}, T_2 = T_U = 500 \text{ K}$

$P_3 = 4 \text{ atm}, q_{2 \rightarrow 3} = 0, T_3 = T_L$

$P_4 = 4.8 \text{ atm}, T_4 = T_L, q_{4 \rightarrow 1} = 0$

NOTE:

T_U (T upper) $\equiv T_H$ (T higher or T hotter)

cyclic process

IV **adiabatic expansion**

III **isothermal expansion**

II **adiabatic compression**

I **isothermal compression**

Carnot refrigerator arithmetic (just negatives of Carnot engine)
for below table see handout

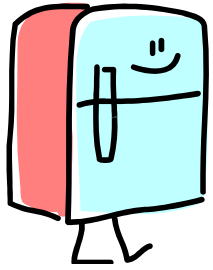
REFRIGERATOR	q	W_{sys}	q_{surr}	
IV. adiabatic expansion $T_H \rightarrow T_L$	0	$-nC_V(T_U - T_L)$	0	work done by system
III. isothermal expansion at T_L $P_4 \rightarrow P_3$	$-nR T_L \ln \frac{P_3}{P_4}$	$+nR T_L \ln \frac{P_3}{P_4} =$ $-nR T_L \ln \frac{P_1}{P_2}$	$-nR T_L \ln \frac{P_1}{P_2}$	work done by sys heat withdrawn from T_L (ice box)
II. adiabatic compression $T_L \rightarrow T_H$	0	$-nC_V(T_L - T_U)$	0	work on system
I. isothermal compression at T_H $P_2 \rightarrow P_1$	$-nR T_U \ln \frac{P_1}{P_2}$	$+nR T_U \ln \frac{P_1}{P_2}$	$+nR T_U \ln \frac{P_1}{P_2}$	heat out at T_H refrig "coils" work on system
net gain/cost		$W_{total} = W_I + W_{II} + W_{III} + W_{IV} =$ $+nR(T_U - T_L) \ln \frac{P_1}{P_2}$	$ q_{out} = -q_{surr_III}$ $+nR T_L \ln \frac{P_1}{P_2}$	$\eta_r \equiv C_R = \frac{-q_{surr_III}}{W_{sys\ total}} = \frac{T_L}{T_U - T_L}$ eqn 5.45 E&R

Coefficient of performance of refrigerator:

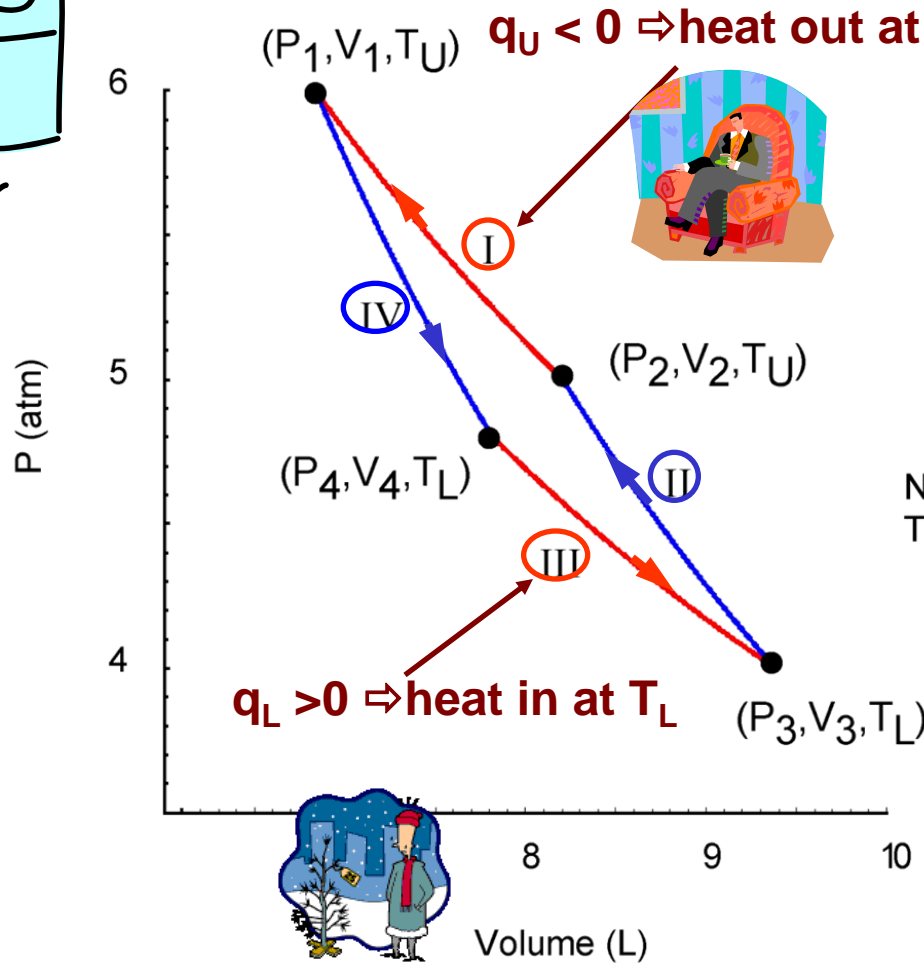
$$\eta_r \equiv C_R = \frac{-q_{surr_III}}{W_{total}} = \frac{q_{III}}{W_{total}} = \frac{T_L}{T_U - T_L}$$

E&R eqn 5.45

reverse Carnot cycle: a heat pump



$W_{\text{sys}} = -W_{\text{surr}} > 0$
work done ON system



$P_1 = 6 \text{ atm}, T_1 = T_U = 500\text{K}$

$P_2 = 5 \text{ atm}, T_2 = T_U = 500\text{K}$

$P_3 = 4 \text{ atm}, q_{2 \rightarrow 3} = 0, T_3 = T_L$

$P_4 = 4.8 \text{ atm}, T_4 = T_L, q_{4 \rightarrow 1} = 0$

NOTE:
 T_U (T upper) $\equiv T_H$ (T higher or T hotter)

cyclic process

- IV **adiabatic expansion**
- III **isothermal expansion**
- II **adiabatic compression**
- I **isothermal compression**

“goodness of performance”

Since refrigerators and heat pumps are just Carnot machines in reverse, the relationship for $\varepsilon = -w_{\text{total}}/q_{\text{I}} = (T_{\text{U}} - T_{\text{L}})/T_{\text{U}}$ holds for these cycles. However only for “engines” does it represent the efficiency or “goodness of performance” (work_{total out}/heat_{in}).

For a refrigerator performance is (heat_{in at TL}/work_{total})

$$\eta_r \equiv C_R = \frac{-q_{\text{from freezer}}}{w_{\text{total}}} = \frac{q_{\text{III}}}{w_{\text{total}}} = \frac{T_L}{T_U - T_L} \quad \text{E\&R eqn 5.45}$$

For a heat pump performance is (heat_{out at TU}/work_{total})

$$\eta_{hp} \equiv C_{HP} = \frac{q_{\text{given off to room}}}{w_{\text{total}}} = \frac{-q_{\text{I}}}{w_{\text{total}}} = \frac{T_U}{T_U - T_L} \quad \text{E\&R eqn 5.44}$$

(> 1)

one more important FACTOID about Carnot machine

for complete **reversible** Carnot cycle:

$$\oint dU = \Delta U = 0$$

$$\oint dH = \Delta H = 0$$

$$\oint \bar{d}q_{rev} = q = \neq 0$$

$$\oint \bar{d}w_{rev} = w = \neq 0$$

BUT ALSO LET'S LOOK AT:

$$\oint_{\text{cycle}} \frac{\bar{d}q_{rev}}{T}$$

one more important **FACTOID** about Carnot machine

$$\int_I \frac{dq_{rev}}{T} = \frac{nRT_U \ln \frac{P_1}{P_2}}{T_U}$$

$$\int_{II} \frac{dq_{rev}}{T} = 0 \text{ (adiabatic)}$$

$$\int_{III} \frac{dq_{rev}}{T} = \frac{-nRT_L \ln \frac{P_1}{P_2}}{T_L}$$

$$\int_{IV} \frac{dq_{rev}}{T} = 0 \text{ (adiabatic)}$$

$$\oint_{\text{cycle}} \frac{dq_{rev}}{T} = 0$$

have we uncovered a new state function entropy (S) ??

$$\Delta S = \int dS = \int \frac{dq_{rev}}{T}$$

does it just apply
to ideal gas Carnot cycle ???

Generalization of Ideal Gas Carnot Cycle

1. Our work on the **(reversible)** Carnot Cycle using an ideal gas as the ‘working substance’ lead to the relationship

$$\varepsilon = \frac{-W_{\text{total}}}{q_U} = \frac{T_U - T_L}{T_U}$$

However, the second law applies to machines with any ‘working substance’ and general cycles.

2. The following presentation shows that a **(reversible)** Carnot machine with ‘any working substance’ cannot have $\varepsilon_{\text{rev any ws}} > \varepsilon_{\text{carnot ideal gas}}$.
3. **REVERSING** the directions of the ideal gas and ‘any rev Carnot’ (e.g. Raff, pp 160-162) shows that $\varepsilon_{\text{rev any ws}} = \varepsilon_{\text{carnot ideal gas}}$
4. One can also show (E&R Fig 5.4, Raff 162-164) that any Carnot machine has $\oint dq_{\text{rev}}/T = 0$ and that any reversible machine cycle can be expressed as a sum of Carnot cycles.

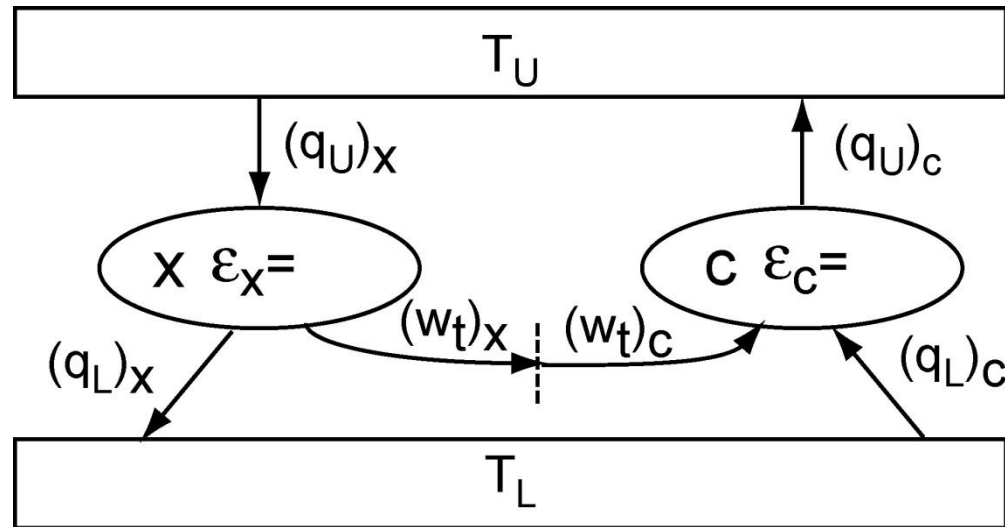
Carnot machine

**Carnot machine: cyclic, reversible, machine
exchanging heat with environment at only
two temperatures T_U , T_L**

Carnot engine: 'forward' Carnot cycle

Carnot heat pump: 'reverse' Carnot cycle

can $\varepsilon_x > \varepsilon_c$ for any Carnot machine X vs ideal gas Carnot machine C ???

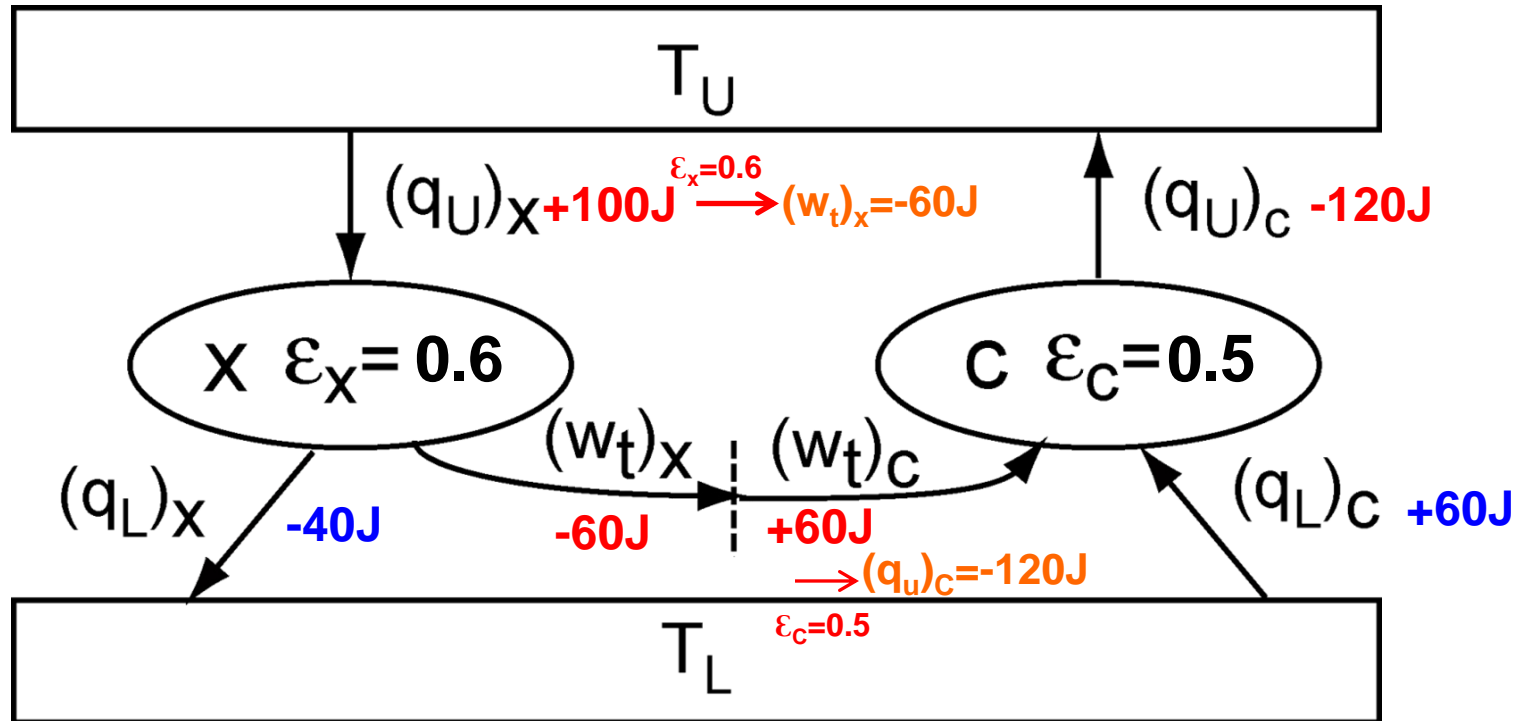


the machine X operates as a Carnot engine doing work, while the machine C operates as a reverse Carnot ideal gas engine acting as a heat pump.

The work **done by X**, $(w_t)_X$ is **used by C**:

$$(w_t)_C = -(w_t)_X$$

?? $\epsilon_x > \epsilon_{\text{Carnot}}$: worksheet for **numerical example** (all w_x goes into w_C)



$$\epsilon = \frac{-W_t}{Q_U} \quad Q_U = \frac{-W_t}{\epsilon} \quad \Delta U = q_U + q_L + w_t = 0$$

$$Q_U = \frac{-W_t}{\epsilon} \quad w_t = -Q_U \epsilon$$

$$W_{\text{total}} = 0$$

$$(q_U)_{\text{total}} = -20\text{J} \quad (\text{into } T_U)$$

$$(q_L)_{\text{total}} = +20\text{J} \quad (\text{out of } T_L)$$

Clausius Statement of Second Law (numerical example)

we assumed an $\epsilon_x > \epsilon_c$ for ideal gas Carnot and calculated

$$W_{\text{total}}=0$$

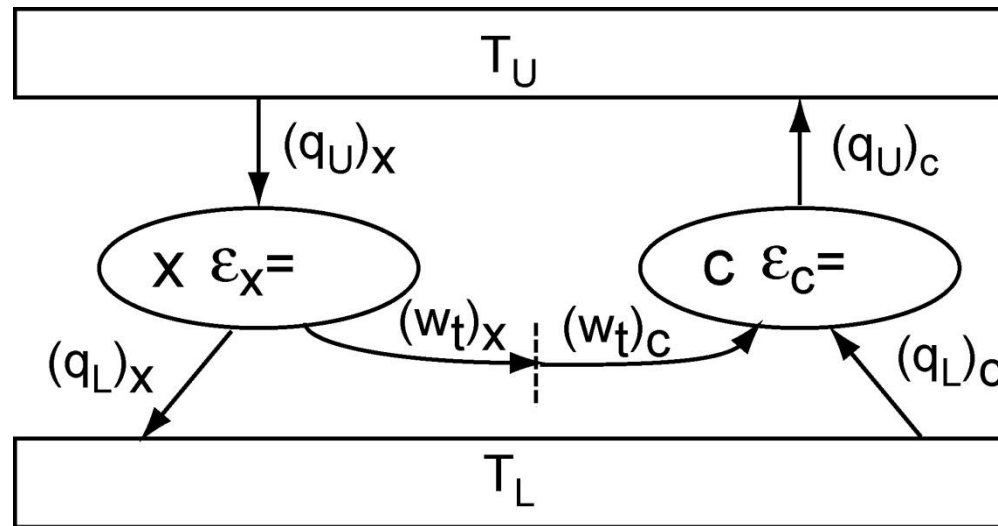
$(q_L)_{\text{total}}=+20\text{J}$ (into 'combo engine'
out of cold reservoir at T_{lower})

$(q_U)_{\text{total}}=-20\text{J}$ (out of 'combo engine'
into heat reservoir at T_{upper})

BUT: It is impossible to have a natural process which produces no other effect than absorption of heat from a colder body and discharge of heat to a warmer body. *Clausius's Statement*

if second law holds $\epsilon_x > \epsilon_c$ cannot be true

general proof: can $\epsilon_x > \epsilon_c$ for Carnot machine X vs ideal gas Carnot machine C ???



$$(q_U)_x > 0$$

$$\epsilon_x = \frac{-(w_t)_x}{(q_U)_x}$$

$$(w_t)_x = -(q_U)_x \epsilon_x$$

$$(q_L)_x + (q_U)_x + (w_t)_x = 0$$

$$(q_U)_c < 0$$

$$\epsilon_c = \frac{-(w_t)_c}{(q_U)_c} = \frac{(w_t)_x}{(q_U)_c}$$

$$(w_t)_x = (q_U)_c \epsilon_c$$

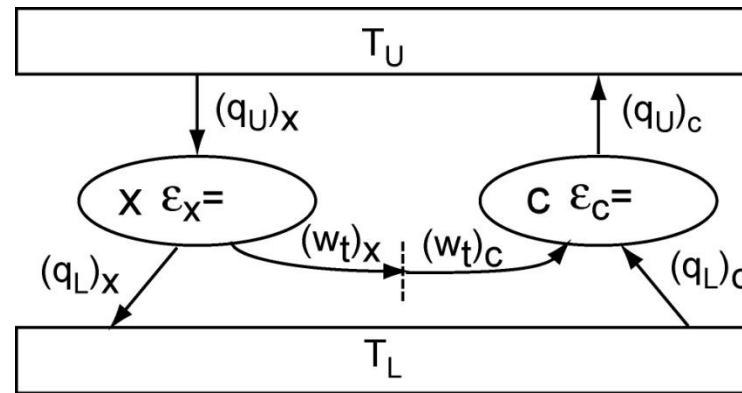
$$(q_L)_c + (q_U)_c + (w_t)_c = 0$$

to give $-(w_t)_x = (w_t)_c$, $\frac{-(q_U)_x}{(q_U)_c} = \frac{\epsilon_c}{\epsilon_x}$, and $(q_U)_c = -\frac{\epsilon_x}{\epsilon_c} (q_U)_x$

$(q_U)_{\text{total}} = (q_U)_x + (q_U)_c = (q_U)_x \left(1 - \frac{\epsilon_x}{\epsilon_c}\right)$ which will be < 0 , for $\epsilon_x > \epsilon_c$

$(q_L)_{\text{total}} = (q_L)_x + (q_L)_c = -(q_U)_x - (w_t)_x + -(q_U)_c + (w_t)_x = -(q_U)_{\text{total}}$

general proof: can $\varepsilon_x > \varepsilon_c$ for Carnot machine X vs ideal gas Carnot machine C ???



So $(q_U)_{\text{total}} < 0$

and

$$(q_L)_{\text{total}} = - (q_U)_{\text{total}} > 0$$

$$\text{with } w_{\text{total}} = (w_t)_x + (w_t)_c = 0$$

so what's the problem ???

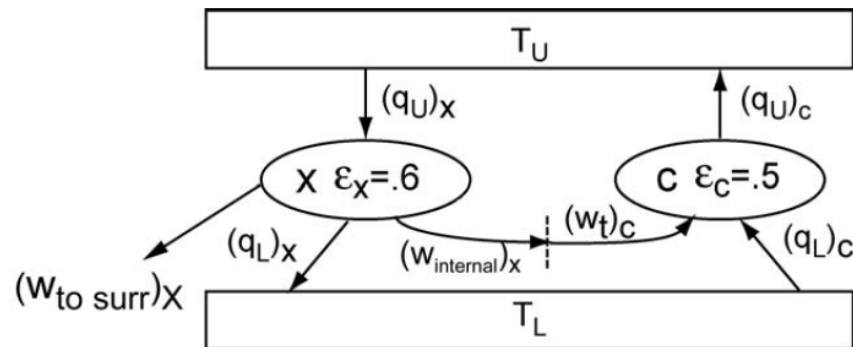
**q transferred $T_L \rightarrow T_U$ with no net work
violates Clausius statement of second law**

so what's the solution ???

$\varepsilon_x > \varepsilon_c$ is not a condition consistent with the Second Law

HW#4 Prob. 23

23. The diagram below, where Carnot engine X and Carnot heat pump C are coupled, is similar to that used in lecture to illustrate that the efficiency of *any* Carnot engine, ϵ_x , has to be the same as that of an ideal gas Carnot engine, ϵ_c , when the engines operate between the same two temperatures. The diagram below differs in that now 33% (-20 J) of the total work done by engine X is done on the surroundings, while 67% (-40 J) is input into the Carnot refrigerator C.



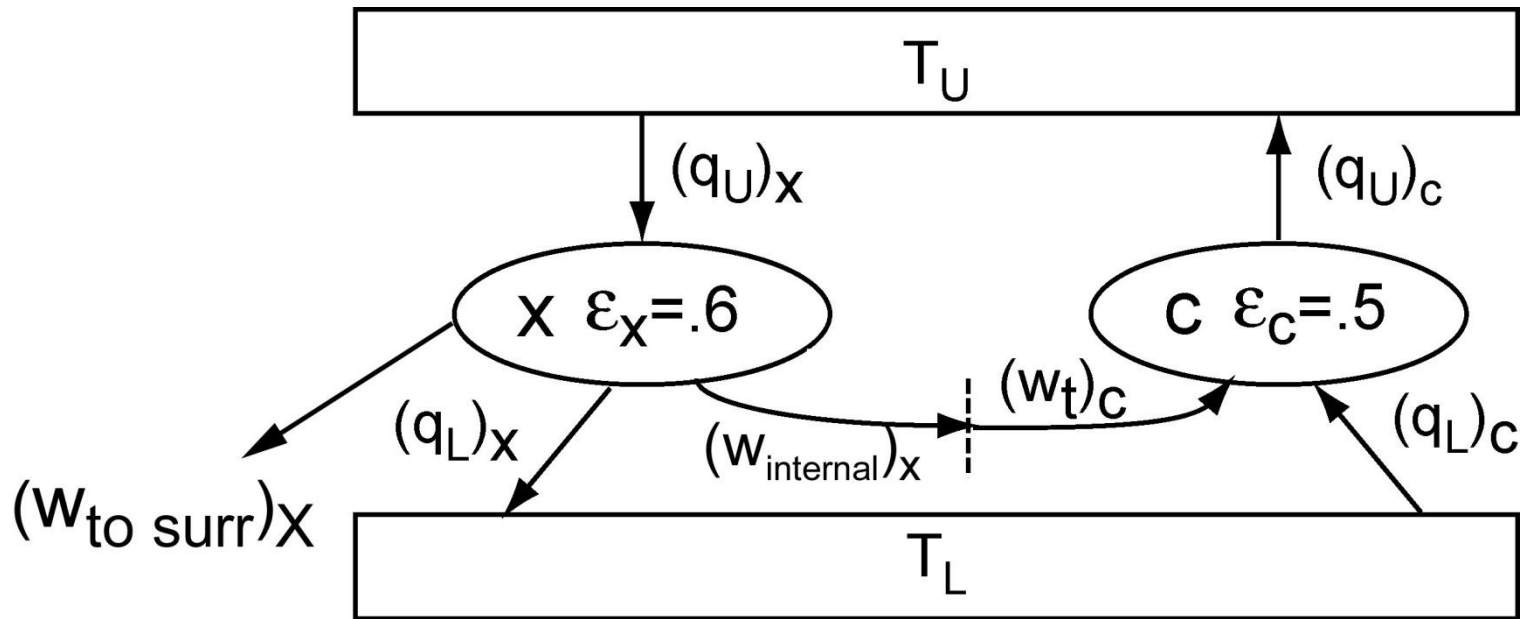
Assume that as indicated $\epsilon_x = 0.6$ and $\epsilon_c = 0.5$.

For $(q_U)_x = 100\text{J}$, $(w_{\text{surr}})_x = -20\text{J}$, $(w_i)_x = -40\text{J}$, $(w_t)_c = +40\text{J}$, and $(q_U)_c = -80\text{J}$

Calculate:

- $(q_L)_x$
- $(q_L)_c$
- $(q_U)_{\text{total}} = (q_U)_x + (q_U)_c$
- $(q_L)_{\text{total}} = (q_L)_x + (q_L)_c$
- $w_{\text{total}} = (w_{\text{surr}})_x + (w_i)_x + (w_t)_c$
- Considering the [correct] results for parts c, d, and e, how does the process with coupled Carnot engines X and C having $\epsilon_x = 0.6$ and $\epsilon_c = 0.5$ violate one of the statements of the Second Law of Thermodynamics

setup for (HW prob #23) ϵ_x efficiency greater than Carnot



$$\epsilon_x = 0.6 \quad (q_U)_x = 100\text{J} \quad \Rightarrow \quad (w_{\text{total}})_x = -60\text{J}$$

$$\epsilon_c = 0.5 \quad (w_{\text{total}})_c = +40\text{J} \quad \Rightarrow \quad (q_U)_c = -80\text{J}$$

$$(w_{\text{sys to surr}})_x = -20\text{J} \quad (w_{\text{internal to C}})_x = -40\text{J}$$

calc: $(q_L)_x$, $(q_L)_c$,
 $(q_L)_{\text{total}}$, $(q_U)_{\text{total}}$, $(w)_{\text{total}}$

ANOTHER CONSEQUENCE OF ASSUMING $\epsilon_x > \epsilon_c$ (2nd Law Statements)

generalization to arbitrary cycle (E&R Fig. 5.4, Raff Fig. 4.11)

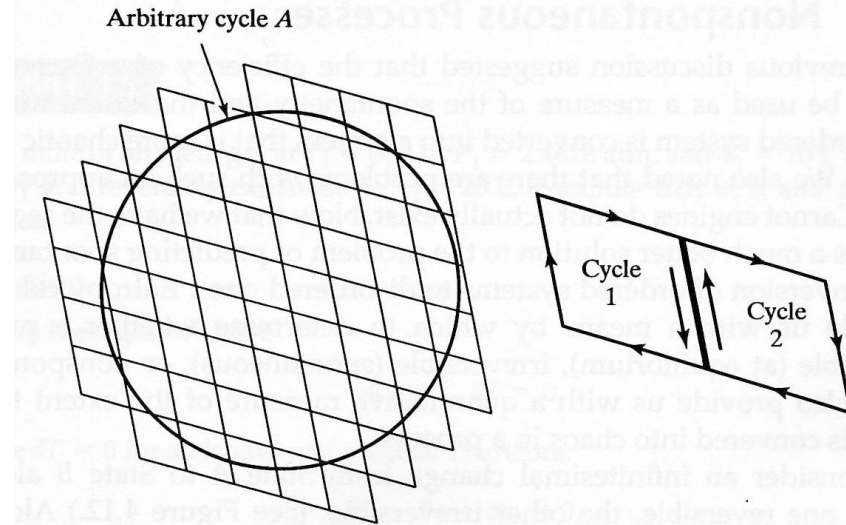
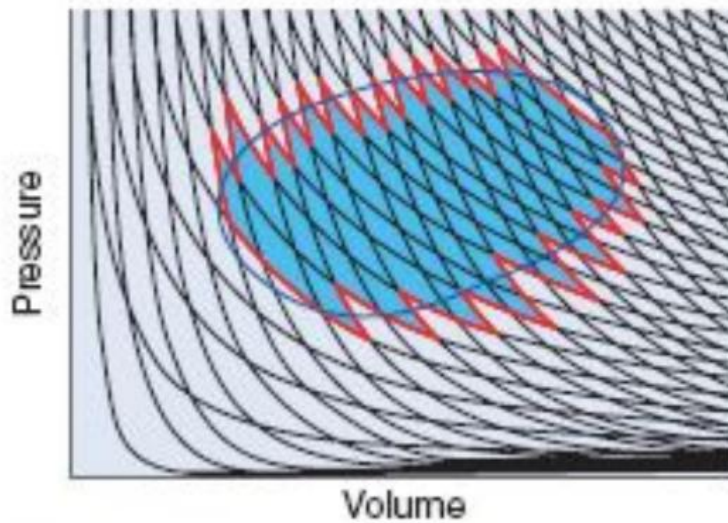


FIGURE 5.4

An arbitrary reversible cycle, indicated by the ellipse, can be approximated to any desired accuracy by a sequence of alternating adiabatic and isothermal segments.

a REALLY BIG RESULT: connecting ε and entropy

have shown generally for any reversible **CYCLIC** engine operating between T_U and T_L :

$$\varepsilon = \frac{-w_{total}}{q_U} = 1 - \frac{T_L}{T_U} \quad \text{now}$$

$$-w_{total} = q_U + q_L$$

so

$$\varepsilon = \frac{q_U + q_L}{q_U} = 1 + \frac{q_L}{q_U}$$

thus

$$1 + \frac{q_L}{q_U} = 1 - \frac{T_L}{T_U}$$

$$\frac{q_L}{T_L} + \frac{q_U}{T_U} = 0 \quad \text{FOR THE CYCLE}$$

(ANY reversible cyclic process operating between T_U and T_L)

the BOTTOM LINE

so generally for this
reversible cycle

DEFINE: $dS \equiv \frac{\bar{d}q_{\text{reversible}}}{T}$

$$\oint dS = \oint \frac{\bar{d}q_{\text{reversible}}}{T} = 0$$

and S is **STATE FUNCTION**

roadmap for second law

- ✓ 1. Phenomenological statements (what is ALWAYS observed)
- ✓ 2. Ideal gas Carnot [*reversible*] cycle efficiency of heat → work (Carnot cycle transfers heat only at T_U and T_L)
- ✓ 3. Any cyclic engine operating between T_U and T_L must have an equal or lower efficiency than Carnot OR VIOLATE one of the phenomenological statements (observations)
- ✓ 4. Generalize Carnot to any reversible cycle (E&R fig 5.4)
- ✓ 5. Show that for this REVERSIBLE cycle

$$q_U + q_L \neq 0 \text{ (}\vec{d}q \text{ inexact differential)}$$

but

$$\frac{q_U}{T_U} + \frac{q_L}{T_L} = 0 \text{ (something special about } \frac{\vec{d}q_{rev}}{T} \text{)}$$

- ✓ 6. **STATE FUNCTION S**, entropy and spontaneous changes

(more to come)